

Corrections

Compressed Liquid Densities of Squalane and Pentaerythritol Tetra(2-ethylhexanoate). O. Fandiño, A. S. Pensado, L. Lugo, M. J. P. Comuñas,* and J. Fernández, *J. Chem. Eng. Data* **2005**, *50*, 939–946.

In this paper, experimental densities were reported for squalane and pentaerythritol tetra(2-ethylhexanoate), PEB8, in the compressed liquid state over the temperature range from (278.15 to 353.15) K and for pressures up to 45 MPa using an Anton Paar DMA 512P vibrating tube densimeter. The dynamic viscosity of PEB8 and squalane at 303.15 K and 0.1 MPa were around 60 mPa·s and 20 mPa·s, respectively. The Anton Paar DMA 512P shows systematic deviations depending on the fluid viscosity. In the original paper, an equation recommended by Anton Paar for the DMA 512P model densimeter was used to calculate the correction factor, $\Delta\rho$. Nevertheless, after the publication of the paper, Anton Paar informed us that the following considerations should be taken into account: (a) the validity range of their equation is for viscosities lower than 100 mPa·s; (b) for viscosities higher than 400 mPa·s, the correction factor becomes constant and equal to $5 \cdot 10^{-4} \text{ g}\cdot\text{cm}^{-3}$; (c) between 100 and 400 mPa·s, the correction factor follows an intermediate behavior.

Supporting Information Available:

New tables and fit parameters that incorporate these viscosity corrections. This material is available free of charge via the Internet at <http://pubs.acs.org>.

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Temperature Effect on the Liquid–Liquid Equilibria for the Some Aliphatic Alcohols + Water + K₂CO₃ Systems. Alireza Salabat* and Mahmood Hashemi, *J. Chem. Eng. Data* **2006**, *51*, 1194–1197.

Page 1196. The binodal curve data for the 2-methyl-2-propanol (1) + water (2) + K₂CO₃ (3) system in Table 5 was published incorrectly. The correct data are shown below.

Table 5. Binodal Curve Data of Mass Fraction for Aliphatic Alcohols (1) + Water (2) + K₂CO₃ (3) at 298.15 K

100 w ₁	100 w ₃	100 w ₁	100 w ₃
2-Methyl-2-propanol + Water + K ₂ CO ₃			
55.0	0.4	20.2	5.9
45.0	1.1	15.5	7.5
37.5	2.2	11.5	9.8
25.8	4.3	8.3	11.9

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